

B/S 5. (Amended) A process according to claim 31, in which Si/T of the modified zeolite is at most 300.

6. (Amended) A process according to claim 31, in which T is aluminium (Al).

7. (Amended) A process according to claim 31, wherein the EU-1 zeolite is obtained by synthesis using at least one solution of an acid.

C1
Cond 8. (Amended) A process according to claim 31, wherein the zeolite is obtained using at least one heat treatment of a EU-1 zeolite obtained by synthesis followed by at least one treatment with a solution of an acid.

9. (Amended) A process according to claim 31, in which the EU-1 zeolite is obtained by dealuminating by at least one heat treatment followed by at least one treatment using a chemical dealuminating compound which is ammonium hexafluorosilicate, silicon tetrachloride, or ethylenediaminetetra-acetic acid, optionally in its sodium or disodium form.

10. (Amended) A process according to claim 31, in which the EU-1 zeolite is obtained by dealuminating by at least one treatment with a chemical dealuminating compound which is ammonium hexafluorosilicate, silicon tetrachloride, or ethylenediaminetetra-acetic acid, optionally in its sodium and disodium form.

C2 12. (Amended) A process according to claim 31, wherein the ^{CATLYST}zeolite comprises at least one matrix and 0.5% to 99.5% by weight of EU-1 zeolite with respect to the matrix + zeolite mixture.

C3 17. (Amended) A process according to claim 31, in which the hydro-

dehydrogenating element is niobium and/or rhenium.

C3
C4
19. (Amended) A process for improving the pour point of a feed comprising paraffins containing more than 10 carbon atoms, in which process the feed to be treated is brought into contact with a catalyst based on EU-1 zeolite, at least partially in its acid form, and at least one hydro-dehydrogenating element, at a temperature of 170°C to 500°C, a pressure of 1 to 250 bar and at an hourly space velocity of 0.05 to 100 h⁻¹, the presence of hydrogen in a proportion of 50 to 2000 l/l of feed.

C5
30. (Amended) A process according to claim 19, in which the compound to be treated is present in a hydrocarbon feed selected from the group consisting of middle distillates, gas oils, vacuum residues, hydrocracking residues, paraffins from the Fischer-Tropsch process, synthesized oils, gas oil cuts and FCC middle distillates, oils, and polyalphaolefins.

Please cancel claims 1, 11, 13-16, 18 and 24 without prejudice or disclaimer.

Please add new claim 31 as follows:

C6
--31. (New) A process for improving the pour point of a feed comprising paraffins containing more than 10 carbon atoms, comprising contacting the feed with a catalyst based on EU-1 zeolite, at least partially in its acid form, and at least one hydro-dehydrogenating element, wherein the EU-1 zeolite comprises silicon and an element T which is Al, Fe, Ga, or B, produced by a process in which at least a portion of elements T are removed from a starting zeolite, whereby the modified zeolite has a global atomic ratio Si/T higher than that of the starting zeolite, by at least 10% of the Si/T ratio of the starting zeolite.--